



# Effects of Angular Fillers on Thermal Runaway of Lithium-Ion Battery



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By adding 1 wt% damage homogenizer (DH), i.e. carbon black microparticles, into the electrodes of lithium-ion batteries, thermal runaway can be mitigated as the battery cells are subjected to impact loadings. In a drop tower test, the generated heat of the modified cells is reduced by nearly 40%, compared with the reference cells. This phenomenon may be attributed to the weakening effect of the carbon black fillers. The shape of the filler grains does not have a pronounced influence on the temperature profile.

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## 1. Introduction

For a large number of engineering applications, among the relevant energy storage approaches, lithium (Li) ion batteries are of the highest specific energy and the lowest specific cost<sup>[1]</sup>. For instance, by using the BacPac model<sup>[2]</sup>, it can be assessed that at the cell level, a LiNi<sub>0.5</sub>Mn<sub>0.3</sub>Co<sub>0.2</sub>O<sub>2</sub> (NMC-532) battery costs ~110 \$/(kW h) and stores ~200 W h/kg. Compared with lead–acid and nickel–metal hydride (NiMH) batteries, the specific cost is lower and the specific energy is higher by 2–5 times<sup>[3]</sup>. The specific cost of a supercapacitor is around 10–20 \$/W · h, and the specific energy is much lower, only a few W h/kg<sup>[4]</sup>. Many other advanced energy storage and energy management technologies, such as fuel cells, are still in the early stage of research and development<sup>[5]</sup>.

Recently, the robustness of Li-ion batteries drew increasing attention<sup>[6]</sup>. Under an ordinary working condition, with the well-developed battery thermal management system (BTMS) as well as battery management system (BMS), a Li-ion battery pack can continuously work for a few years. Under adverse conditions, e.g. if the battery is over-charged, over-heated, or heavily impacted, drastic temperature increase can occur, associated with the thermally-accelerated exothermic reactions. For small battery cells, due to the

rapid heat transfer through the cell cases, the peak temperature may remain in the safe range. For large-scale energy storage systems, thermal runaway could take place; the peak temperature can rise to above a few hundred degrees in a few minutes, and eventually the batteries may catch on fire<sup>[7]</sup>. It imposes tough safety challenges<sup>[8]</sup>, as the electrolytes in Li-ion batteries are highly flammable<sup>[9]</sup>. In order to understand and enhance the system robustness in harsh environments, heat generation characteristics of mechanically abused Li-ion battery cells must be investigated.

A common cause of thermal runaway is internal shorting. The cathode and the anode in a Li-ion battery cell should not contact each other, and are usually separated by a porous membrane. To minimize energy loss, the distance between the electrodes is kept as small as possible. The membrane thickness is typically only 10–30 μm<sup>[10]</sup>. The membrane is often made of polymers, such as polystyrene and polypropylene, and of a high porosity. Such a thin, highly porous polymer membrane can relatively easily rupture as the battery cell is impacted; hence, the cathode and the anode active materials directly react with each other, generating a large current and rapidly releasing a large amount of thermal energy<sup>[11]</sup>.

Directly preventing internal shorting is difficult, since there are tight constraints on the cost, weight, thickness, stability, and durability of the membrane. People have investigated a few indirect thermal-runaway mitigation concepts, including positive thermal coefficient (PTC) materials<sup>[12]</sup>, phase transfer materials (PTM)<sup>[13]</sup>, and low-melting-point (LMT) membranes<sup>[11]</sup>. Most of them involve

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mechanisms that increase the internal impedance. For example, when internal shorting occurs and the temperature rises, a PTC material can largely increase the electrical resistivity of the electrode, which blocks the return path of the internal short circuit.

Recently, a new concept, damage homogenizer (DH), was proposed: By adding a small amount of DH in electrode, when the battery cell is impacted, widespread damaging is triggered, which would raise the internal impedance and lower the heat generation rate. Once the heat generation is balanced by the heat transfer, the local temperature increase would cease. The DH can be multiwall carbon nanotube bundles<sup>[14]</sup> or smooth microparticulates<sup>[15]</sup> that are uniformly distributed and relatively weakly bonded with the active materials. Compared with the PTC technique, the DH takes effect early and fast. The electrode is damaged immediately as the battery is impacted, even before the thermal runaway begins; the damaging procedure is completed in a few microseconds, which is much faster than the temperature rise.

A few key design parameters have been analyzed, including the DH content. However, the effects of the DH configuration, particularly the particle shape, are still quite unclear. On the one hand, if DH microparticulates (DHMP) are smooth, the slurry processing is easier, primarily due to the “ball bearing” effect<sup>[7]</sup>; thus, the efficiency of additives is amplified. On the other hand, if DHMP are angular, the sharp corners may serve as stress concentration sites that weaken the modified electrode; as a result, widespread damaging may occur smoothly. In the current study, we carried out nail penetration and blunt impact experiments on Li-ion battery coin cells modified by angular DHMP, so as to examine which process is more important.

The current study will be focused on small-sized coin cells. In the early stage of heat generation in an impact test, the electrochemical reactions associated with temperature increase in a small coin cell and a large pouch cell are similar. Compared with the late stage, in the early stage before the temperature approaches the critical level, the reactions are more relevant to thermal-runaway mitigation; therefore, the coin-cell testing sheds much light on our future investigation on large-scale energy storage systems.

## 2. Experimental

Reference cathode was processed by using  $\text{LiNi}_{0.5}\text{Mn}_{0.3}\text{Co}_{0.2}\text{O}_2$  (NCM; Product No. NCM-04ST, TODA America) as the active material, carbon black (CB; Product No. CENERGY-C65, TIMCAL) as the conductive agent, and polyvinylidene fluoride as the binder (PVDF; Product No. 182702, Sigma-Aldrich). The average molecular weight of the PVDF was about 534,000. Fig. 1 depicts the cell structure. Nearly 10 g of the components were thoroughly mixed in an agate mortar with the NCM-CB-PVDF mass ratio of 93:3:4, and dissolved in N-methyl-pyrrolidone (NMP; Product No. 328634, Sigma-Aldrich).

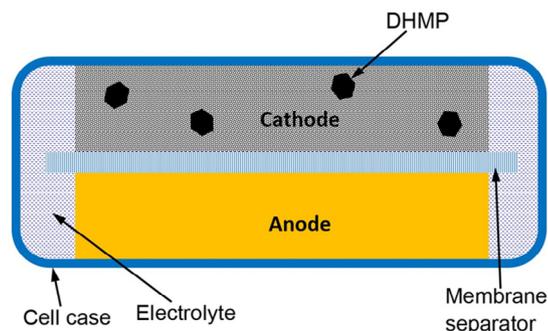


Fig. 1. Schematic of the coin-cell structure.

The mass ratio of the powder to NMP was 10:4. Sonicator (Model Q55, Qsonica) was employed to form slurry at the 60% power level for 30 min. The slurry was distributed by a film applicator (EQ-Se-KTQ-100, MTI) with a thickness of about 200  $\mu\text{m}$  on a 20  $\mu\text{m}$  thick aluminum (Al) current collector, and dried in a vacuum oven at 100  $^{\circ}\text{C}$  for 24 h. The dried slurry was compressed to about 2/3 of its original thickness through calendaring, by using a hardened tool steel rolling mill. The final density of the cathode layer was about 3.2  $\text{g}/\text{cm}^3$ . Reference anode was produced by using artificial graphite (AG; EQ-Lib-CMSG, MTI), CB, and PVDF, with the mass ratio of 93:1:6. The procedure was similar to that of the cathode, except that the current collector was a 20  $\mu\text{m}$  thick copper (Cu) foil. The final thickness of cathode was  $\sim 100$   $\mu\text{m}$  and the final thickness of anode was  $\sim 50$   $\mu\text{m}$ . Similar slurry processing approaches were employed to fabricate DHMP-modified cathodes and anodes, with Darco-KBG angular carbon black microparticles being added into the powder mixture. The DHMP grain size was sieved to 45–53  $\mu\text{m}$ ; its amount was 1 wt.% of the total electrode mass. Fig. 2 shows typical SEM images of DHMP and DHMP-modified cathode and anode materials.

Full cells were prepared for impact and nail tests. The cathode and anode were cut into 14.3 mm diameter disks. To match the

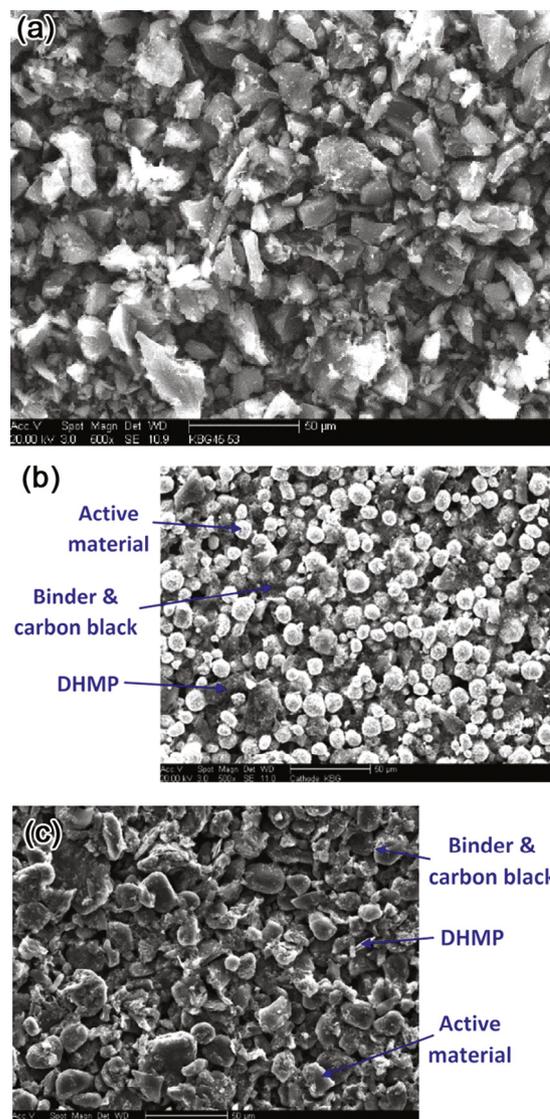


Fig. 2. Typical SEM images of (a) DHMP, (b) DHMP-modified cathode, and (c) DHMP-modified anode.

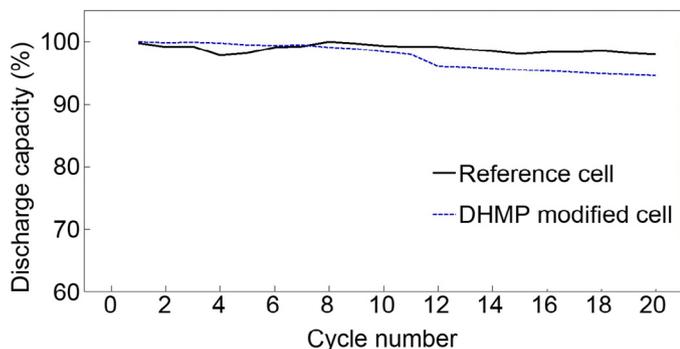


Fig. 3. Typical cycling performance of reference and DHMP-modified cells.

capacity, the active material mass in an anode was nearly 20 mg, ~50% of that of the cathode. In a 2016 battery coin cell case, by using a stainless steel spring spacer, a cathode disk was pressed on a trilayer polypropylene–polyethylene (PP/PE/PP) membrane (Product No. 2320, Celgard), supported by an anode disk. About 30  $\mu\text{L}$  electrolyte (BASF, 1 mol/L  $\text{LiPF}_6$  in 1:1 EC–EMC) was added, and the cell was sealed by a MTI CR2016 crimping machine at 800 psi (5.516 MPa). All coin cells were rested at room temperature for 24 h, and charged and discharged for a few cycles by a MTI BST8-3 Analyzer to ensure that the full capacity was reached.

To test the effects of DHMP on cathodes, cathode half-cells were assembled by replacing the anode layer by a 1.1 mm thick, 15.4 mm diameter lithium disk. The electrochemical performance of the half-cells was examined by the MTI BST8-3 Analyzer, after they had been rested for 24 h at room temperature. Typical curves are shown in Fig. 3. The voltage range was 3–4.3 V; the charge–discharge rate was 1C. Reference half-cells were assembled through a similar procedure, except that cathodes did not contain DHMP.

Reference and DHMP-modified full cells were fully charged to 4.6 V at 0.1C, and tested in nail penetration (NP) and impact experiments. In a NP test, a 1.59 mm diameter stainless steel nail was driven by a table-top vise through a charged battery cell, with a constant speed of ~0.5 mm/s. Impact test was performed by dropping a 7 kg cylindrical steel hammer onto the battery cell. The drop distance was 15 cm. A 6.35 mm diameter brass bead was placed at the center of the top surface of the battery cell, so as to create a heterogeneous loading. In both NP and impact tests, the cell temperature was continuously measured by an Omega TT-K-40-25 type-K gage 40 thermocouple equipped with an Omega OM-EL-USB-TC temperature logger data acquisition system, with the accuracy of  $\pm 0.5$   $^{\circ}\text{C}$  and the record interval of 1 s. The battery cell was insulated by a 25 mm thick circular Durometer-90A polyurethane clamp from the top and a 12.5 mm thick circular Durometer-75D polyurethane plate from the bottom, having 9.5 mm diameter circular hole in the middle. The thermocouple was fixed by a duct tape at the bottom surface of the cell, 5 mm away from the center. The cell was mounted on the bottom plate by 3 layers of insulating tapes. After the NP or impact test, the battery cell was opened up and the damaged cathode and anode layers were examined. The experimental results are shown in Figs. 4–7. The variation of peak temperature of nominally same samples was less than the resolution of the measurement system, for all the testing cases under investigation.

### 3. Results and Discussion

The SEM image in Fig. 2 shows the DHMP grains. The maximum grain size is ~50  $\mu\text{m}$ , comparable with yet smaller than the cathode and anode layer thickness. Thus, the DHMP distribution is somewhat

two-dimensional (2D). The overall concentration of DHMP is 1%; the linear number density is ~10%. They are quite uniformly mixed with NCM and AG particles.

Carbon black and DHMP mainly differ in grain size. To reach a high conductivity among adjacent active material grains, the CB particle size is much smaller, on the nanometer (nm) scale. The DHMP grain size is larger, so that when the electrode is impacted, sufficient energy can be stored and trigger DHMP–matrix debonding<sup>[16]</sup>. Fig. 2(a) indicates that the grain shape of DHMP is quite irregular.

When the DHMP content is relatively high, higher than 1.5–2 wt.%, the cycling performance of the modified cells is quite poor, likely caused by the electrolyte absorption and swelling of the large DHMP. With a relatively low DHMP content below 1 wt.%, the addition of DHMP does not have a significant influence on the cycling performance (Fig. 3), as it should, since the chemical composition of DHMP is similar with CB. The first-cycle Coulombic efficiency is around 88% for both DHMP modified cathode half-cell and reference half-cell. In the first dozen of charge–discharge cycles, the capacities of reference and modified cells decrease by 2%–5%. For the modified cell, there is a drop in capacity at the 8th cycle, which may be attributed to the difference in volume changes of NCM and DHMP microparticles, resulting in certain initial configuration changes in the initial few cycles.

In a full-cell nail test, as the cell is penetrated by the electrical conductive nail, the membrane separation is broken apart and the cathode and the anode form a short circuit. The internal shorting causes a large current and a rapid heat generation, so that the local temperature rises in 10–20 s. In a large pouch cell, the temperature would keep increasing to more than 100  $^{\circ}\text{C}$ , due to the difficulty in heat transfer in the interior of the cell<sup>[11]</sup>. As the cell temperature is relatively high, more aggressive exothermal reactions are triggered and the temperature increase is accelerated, i.e. thermal runaway would take place<sup>[17]</sup>. Eventually, the highly flammable electrolyte can be ignited, resulting in a catastrophic system failure. In the current study, because the surface area to volume ratio of the small coin cell is quite large, heat conduction rate is high. Therefore, as the temperature increase,  $\Delta T$ , is 5–6  $^{\circ}\text{C}$ , heat accumulation is balanced by heat transfer, and the cell temperature reaches the peak value. With the electrical energy being continuously consumed, after ~20 s the temperature begins to decrease, forming a long tail section in the temperature profile. The tail length is 10–20 min, before  $\Delta T$  converges to zero. The average temperature decrease rate is ~0.5  $^{\circ}\text{C}/\text{min}$ . Fig. 4 suggests that the nail penetration responses of the reference cell and the DHMP-modified cell are quite similar. The initial temperature increase rate, the peak temperature, and the post-peak temperature reduction rate do not exhibit any significant difference. The DHMP-modified cell has a slightly higher peak temperature, as addition of DHMP increases

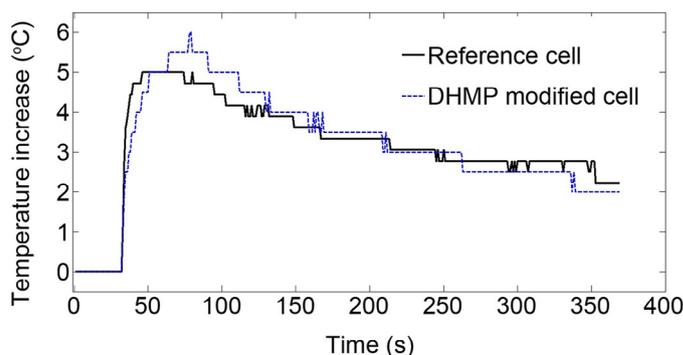
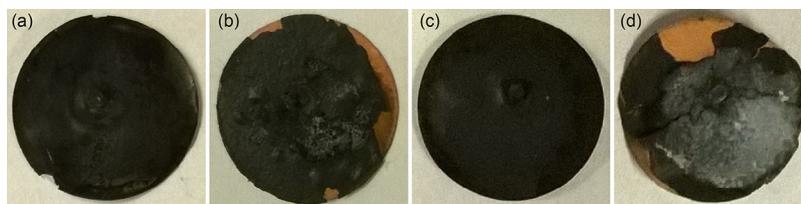


Fig. 4. Typical temperature profiles in nail penetration tests.

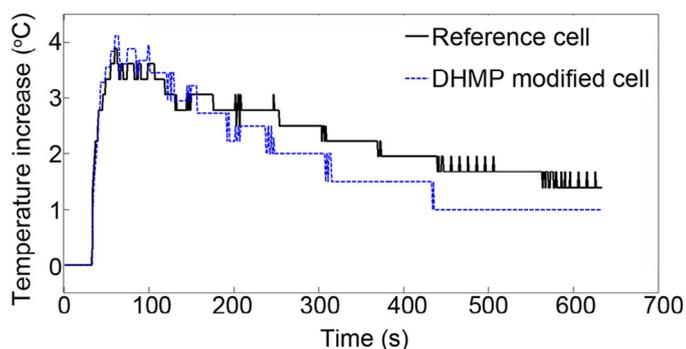


**Fig. 5.** Photos of cell components after nail penetration tests: (a) cathode and (b) anode layers from a reference cell; (c) cathode and (d) anode layers from a DHMP-modified cell.

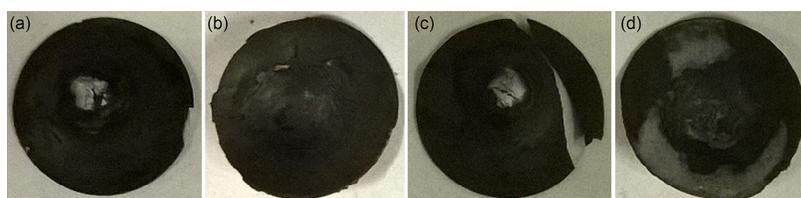
the conductivity of electrode. Clearly, because nail penetration occurs at a slow loading rate, the damage promotion effect of DHMP is negligible.

Fig. 5 shows typical damaged cathode and anode layers of reference and DHMP-modified cells after nail penetration. The reference and the modified cathodes are nearly the same, agreeing with the temperature profile measurement results. The modified anode contains more evident markings of electrochemical reactions (the whitened areas). The whitened area is covered by lithium hydroxide generated by the reactions between the lithiated carbon and  $H_2O$ , after the cell is open and the components are exposed to air. It is possible that the anode can be more aggressively weakened by DHMP than the cathode, and therefore, when the local temperature is higher, the swelling and softening of PVDF binder as well as the associated electrolyte motion lead to a larger extent of structural change. However, because the cathode is the dominant component of heat generation and the anode effects are secondary<sup>[11]</sup>, the temperature profile is not affected.

In the impact test, the temperature profile of the reference cell is somewhat similar to that of the NP test (Fig. 6). The cell temperature rapidly increases to the peak value, followed by a gradual decay, indicating that upon the hammer impact, the highly porous, thin polymer membrane separator ruptures, so that the cathode and anode are in direct contact and the short circuit aggressively releases and dissipates the stored electrical energy. Because the conductivity of the active materials is lower than that of stainless steel nail, compared with the NP test the heat generation rate is



**Fig. 6.** Typical temperature profiles in impact tests.



**Fig. 7.** Photos of cell components after impact tests: (a) cathode and (b) anode layers from a reference cell; (c) cathode and (d) anode layers from a DHMP-modified cell.

relatively slow. Consequently, the initial temperature increase rate, the peak temperature, and the duration of high-temperature plateau are lower than those of the NP test. The tail section of the temperature profile lasts longer, since the total stored electric energy is not related to the cell testing method.

As DHMP is added in the electrodes, the response of the modified cell in the impact test is different from that of the reference cell. While the initial temperature rise and the peak temperature are similar, the temperature reduction rate,  $\alpha$ , in the tail section is much lowered. For a reference cell,  $\alpha$  is  $\sim 0.2$  °C/min. For a modified cell,  $\alpha$  is  $\sim 0.3$  °C/min, nearly 50% higher. The total heat generation,  $U$ , can be calculated as the area under the temperature profile curve, since the specific heats of cell components do not vary during the impact test. The value of  $U$  of the reference cell is  $\sim 40\%$  higher than that of the modified cell. It is clear that DHMP suppresses heat dissipation, which should be attributed to the widespread damaging of the modified cathode. As the DHMP raises the local stress level and also because of the large stiffness mismatch between the DHMP and the NCM matrix, the material morphology is greatly changed when the electrode is impacted. However, compared with the battery cells modified by relatively smooth fillers<sup>[15]</sup>, the change in temperature profile is at the same level, implying that the DHMP shape may not be a vital factor. That is, the effects of the smooth slurry processing and the higher level of stress concentration are balanced by each other, for the systems under investigation; factors other than filler shape may be more important. Such factor includes the mismatch of the stiffness of the DHMP and the electrode matrix; the porosity, which determines the effective bulk modulus; and the surface free energy, which dominates the interfacial bonding between the DHMP and the matrix.

As shown in Fig. 7, the features of reference and modified anodes are similar to that of the NP test, and they may not be the dominant factors of heat generation. The modified cathode is weakened by DHMP and upon the impact loading, much more severe damages take place. It may not directly affect the membrane rupture sites, but would raise the resistivity of the surrounding electrode, i.e. the return path.

#### 4. Concluding Remark

To summarize, addition of 1 wt% angular carbon black microparticles into the cathode and the anode of a lithium-ion battery cell does not affect the cycling performance. In a nail

penetration test, the cathode behaviors of the reference cell and the modified cell are similar; the anode of the modified cell demonstrates signs of more aggressive electrochemical reactions, which however, does not influence the temperature profile. In an impact test, the anode performance is similar to that of the nail test; the modified cathode is much weakened and thus, suppresses the heat generation. The generated heat is reduced by ~40% in the modified cell; the peak temperature does not vary much. For the battery systems under investigation, the shape of the filler grains does not play a critical role in the internal shorting process. These findings shed light on the development of thermal-runaway mitigation techniques.

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### References

- [1] M. Broussely, G. Archdale, J. Power Sources 136 (2004) 386–394.
- [2] P.A. Nelson, K.G. Gallagher, I. Bloom, D.W. Dees, Modeling the Performance and Cost of Lithium-ion Batteries for Electric-drive Vehicles (No. ANL-11/32), Argonne National Laboratory, Argonne, IL, 2011.
- [3] M. Lowe, S. Tokuoka, T. Trigg, G. Gereffi, Lithium-ion Batteries for Electric Vehicles: The US Value Chain, Duke University Center on Globalization, Governance & Competitiveness, 2010.
- [4] I. Hadjipaschalis, A. Poulidakis, V. Efthimiou, Renew. Sustain. Energy Rev. 13 (2009) 1513–1522.
- [5] S. Wasmus, A. Küver, J. Electroanal. Chem. 461 (1999) 14–31.
- [6] P.G. Balakrishnan, R. Ramesh, T.P. Kumar, J. Power Sources 155 (2006) 401–414.
- [7] Q. Wang, P. Ping, X. Zhao, G. Chu, J. Sun, C. Chen, J. Power Sources 208 (2012) 210–224.
- [8] H. Maleki, G. Deng, A. Anani, J. Howard, J. Electrochem. Soc. 146 (1999) 3224–3229.
- [9] G.H. Kim, A. Pesaran, R. Spotnitz, J. Power Sources 170 (2007) 476–489.
- [10] S.S. Zhang, J. Power Sources 164 (2007) 351–364.
- [11] J.T. Lundquist, C.B. Lundsager, N.I. Palmer, H.J. Troffkin, U.S. Patent No. 4, 731,304, 1988.
- [12] X.M. Feng, X.P. Ai, H.X. Yang, Electrochem. Commun. 6 (2004) 1021–1024.
- [13] S.A. Khateeb, M.M. Farid, J.R. Selman, S. Al-Hallaj, J. Power Sources 128 (2004) 292–307.
- [14] A.V. Le, M. Wang, Y. Shi, D. Noelle, Y. Qiao, W. Lu, J. Appl. Phys. 118 (2015) 085312.
- [15] A.V. Le, M. Wang, Y. Shi, D. Noelle, Y. Qiao, J. Phys. D Appl. Phys. 48 (2015) 385501.
- [16] A.K. Kaw, Mechanics of Composite Materials, CRC Press, Boca Raton, FL, 2005.
- [17] D. Doughty, E.P. Roth, Electrochem. Soc. Interface. 21 (2012) 37–44.